<Provisional translation>

## Roadmap for Carbon Recycling Technologies

June 2019

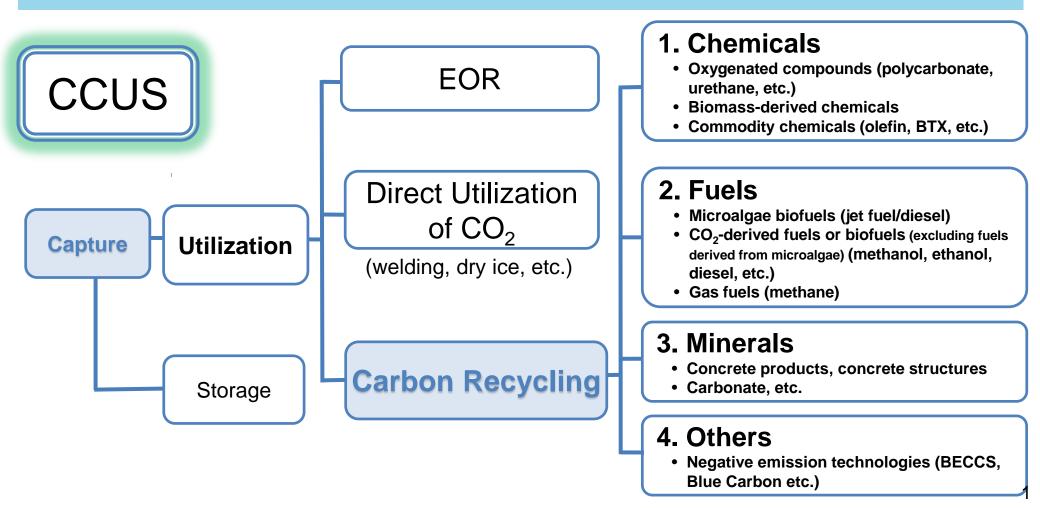
## Ministry of Economy, Trade and Industry

Cooperation of Cabinet Office, Ministry of Education, Culture, Sports, Science and Technology & Ministry of the Environment

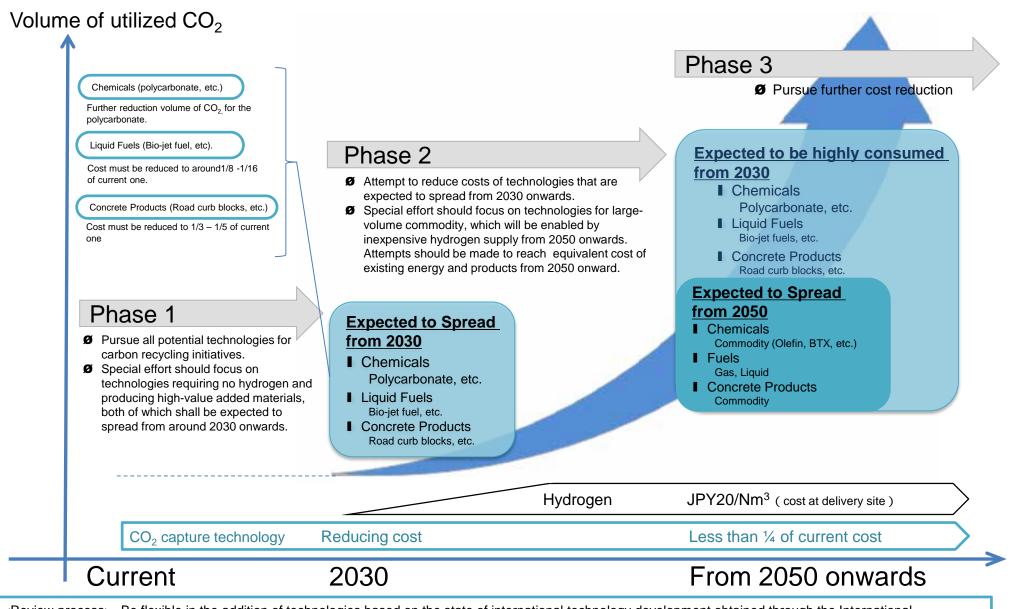
In the event of any doubts arising as to the contents, the original Japanese version is to be the final version.

## **CCUS/Carbon Recycling**

- With the concept of Carbon Recycling technology, we consider carbon dioxide as a source of carbon, and promote capturing and recycling this material. Carbon dioxide (CO<sub>2</sub>) will be utilized for producing recycled materials and fuels by mineralization, artificial photosynthesis and methanation and this will also control CO<sub>2</sub> emissions to the air.
- Carbon Recycling technology advances research and development of CO<sub>2</sub> utilization promoting collaborations among industries, academia and governments around the world and stimulates disruptive innovation.
- Carbon Recycling is one of key technologies for the society, together with energy saving, renewable energy and CCS.



## **Roadmap for Carbon Recycling Technologies**



<Review process> Be flexible in the addition of technologies based on the state of international technology development obtained through the International Conference on Carbon Recycling among Industry-Academia-Government, or proposals of new technologies. The roadmap should be reviewed in five years as needed, take into account the revision of the "Long term Strategy for Growth strategy based on the Paris Agreement (provisional translation)".

## Summary of Carbon Recycling Technologies R&D

1 Price researched by secretariat

2 Basic substances, chemicals(excluding some oxygenated compounds), and many technologies for fuels require large amounts of inexpensive CO<sub>2</sub>-free hydrogens. Biomass-derived fuels may require hydrogen for hydrogenation treatment, etc.

Category	Substance After CO <sub>2</sub> Conversion	Current Status <sup>1</sup>	Challenges	Price of the Existing Equivalent Product <sup>1</sup>	In 2030	From 2050 Onwards
Basic Substance	Syngas/Methanol, etc.	Partially commercialized. Innovative process (light electricity utilization) is at R&D stage	Improvement of conversion efficiency and reaction rate, improvement in durability of catalyst, etc.	-	Reduction in process costs	Further reduction in process costs
Chemicals	Oxygenated Compounds	Partially commercialized (polycarbonates, etc.), Others are at R&D stage [Price example] Price of the existing equivalent product (Polycarbonate)	Reduce the amount of CO <sub>2</sub> emission for polycarbonate. Other than polycarbonate, etc. commercialized (Improvement in conversion rate/selectivity, etc.)	Approx. JPY 300- 500/kg (polycarbonate (domestic sale price))	Costs: similar to those of existing energy/products	Further reduction in costs
	Biomass-derived Chemicals	Technical development stage (non-edible biomass)	Cost reduction/effective pretreatment technique, etc. conversion technologies, etc.	-	Costs: similar to those of existing energy/products	Further reduction in costs
	Commodity Chemicals (olefin, BTX, etc.)	Partially commercialized (Syngas, etc. produced from coal, etc. is utilized)	Improvement in conversion rate/selectivity, etc.	JPY 100/kg (ethylene (domestic sale price))	_	Costs: similar to those of existing energy/products
Fuels	Liquid Fuel (microalgae biofuel)	Demonstration Stage [Price example] Biojet Fuel: JPY 1600/L	Improvement productivity, cost reduction/ effective pretreatment technique, etc.	JPY 100/L level (bio-jet fuel (domestic sale price))	Costs: similar to those of existing energy/products (JPY 100-200/L)	Further reduction in costs
	Liquid Fuel (CO <sub>2</sub> - derived fuels or biofuels (excluding microalgae- derived ones))	Demonstration stage (E-Fuel, etc.), partially commercialized for edible biomass-derived bioethanol	Improvement in current processes, system optimization, etc.	JPY 50-80/L (alcohol as raw material (imported price) JPY approx. 130/L Industrial alcohol (domestic sale price)	_	Costs: similar to those of existing energy/products
	Gas Fuel (Methane)	Demonstration Stage	System optimization, scale-up, etc.	JPY 40-50/Nm <sup>3</sup> (Natural gas (imported price))	Reduction in costs for CO <sub>2</sub> -derived CH <sub>4</sub>	Costs: similar to those of existing energy/products
Minerals	Carbonates/Concrete Products, Concrete Structures	Partially commercialized. R&D for various technologies techniques are underway towards cost reduction. [Price example] order of JPY 100/t (Road curb block)	Separation of CO <sub>2</sub> -reactive and CO <sub>2</sub> - unreactive compounds, comminution, etc.	0	Road curb Block costs: similar to those of existing energy/products	Other products, except road curb block costs: similar to those of existing energy/products
Common Technology	$CO_2$ Capture	Partially commercialized (chemical absorption). Other techniques are at research/ demonstration stage [Price example] Approx. JPY4000/t-CO <sub>2</sub> (Chemical absorption)	Reduction in the required energy, etc.	_	JPY 1000-2000 level /t-CO <sub>2</sub> (chemical absorption, solid absorption, physical absorption, membrane separation)	JPY 1000/t-CO <sub>2</sub> or lower
Basic Substance	Hydrogen	Technologies have been roughly established (water electrolysis, etc.) R&D for other techniques are also underway towards cost reduction.	Cost reduction, etc.		JPY 30/Nm <sup>3</sup>	JPY 20/Nm <sup>3</sup> (cost at delivery site)

### **Scope : Roadmap for Carbon Recycling Technologies**

The carbon recycling technology, where we consider  $CO_2$  as a resource, will begin with a smaller recycle volume. We expect this initiative will continue to expand into different application areas as achieving cost effectiveness. We set relatively short-term targets in 2030 while 2050 onward is seen as a mid- to long-term target.

2030: Technologies aiming at achieving commercialization as early stage as possible.

- (1) Establish an environment that fosters easy utilization of CO<sub>2</sub> (reducing costs for capture and recycle of CO<sub>2</sub>)
- (2) Processes whose basic technology is established can replace existing products by reducing costs

(Products that do not require inexpensive hydrogen supply, as well as high-value added products can replace existing products)

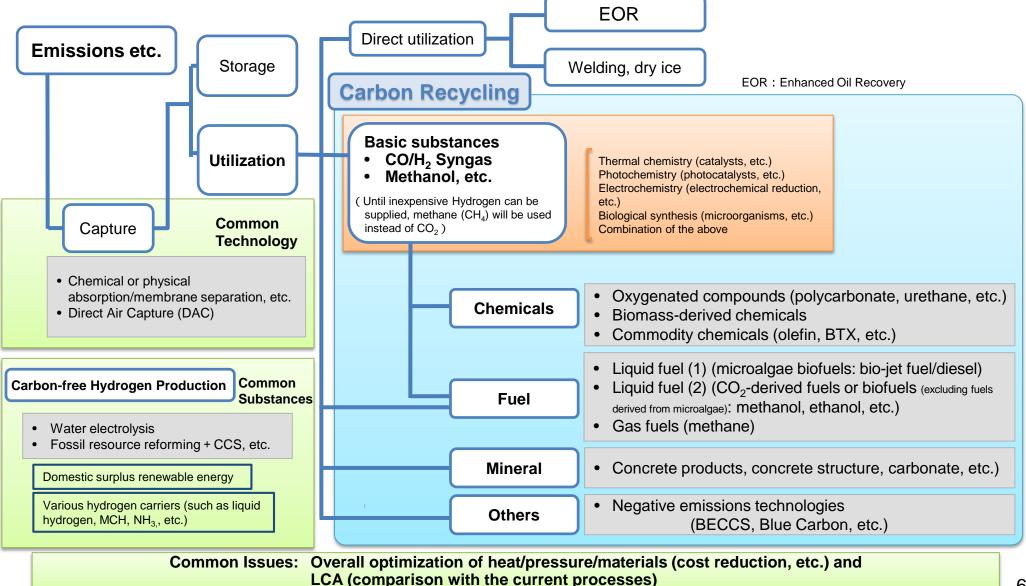
2050: Technologies aiming at achieving commercialization in the mid- to long-term. Early-stage technologies that have greater impacts by using a large amount of CO<sub>2</sub> (enabled by inexpensive hydrogen)

	2030 (short-term)	2050 onward (mid-to long-term)
Field	<ul> <li>Technologies producing high-value added products and/or not requiring inexpensive hydrogen will be commercialized first:</li> <li>Chemicals (polycarbonate, etc.)</li> <li>Liquid fuels (bio-jet fuel, etc.)</li> <li>Concrete products (road curb blocks, etc.)</li> </ul>	<ul> <li>Extended to products that have large demand:</li> <li>Chemicals (commodity: olefin, BTX, etc.)</li> <li>Fuels (gas, liquid)</li> <li>Concrete products (commodity)</li> </ul>

## Individual technologies

## **CCUS/ Carbon Recycling**

■ With the concept of Carbon Recycling technology, we consider carbon dioxide as a source of carbon, and promote capturing and recycling this material. Carbon dioxide (CO<sub>2</sub>) will be utilized for producing recycled materials and fuels by mineralization, artificial photosynthesis and methanation and this will also control CO<sub>2</sub> emissions to the air.



## **Common technology**

## ■ CO<sub>2</sub> Capture Technology

- <Technological Challenges>
- Reduction in capital and operational costs and in required energy
  - Development of new functional materials (absorbents, adsorbents, separation membrane)
  - (improvements in selectivity/capacity/durability improvements) Reduction in production costs of functional materials Optimization of processes(in terms of heat/substance/power, etc.)
- Selection of the types of CO<sub>2</sub> capture technologies based on the CO<sub>2</sub> emission source/application
- Establishing CO<sub>2</sub> capture and conversion systems by matching CO<sub>2</sub> supply and demand with approaching co-production
- Transportation and storage

#### <Individual Technologies>

- Chemical absorption (temperature swing (current process)) Approx. JPY 4,000/t-CO<sub>2</sub> Required energy: Approx.2.5GJ/t-CO<sub>2</sub>
- Physical absorption (pressure swing (demonstration stage))
- Solid absorption (temperature swing) (R&D stage)
- Physical adsorption (pressure/temperature swing, less advantages in scale-up, improvements needed in selectivity/capacity/endurance life)
- Membrane separation (pressure difference)
- Others: cryogenic separation technique, Direct Air Capture, etc.

<Process Technologies to facilitate CO<sub>2</sub> Capture>

- Oxygen-enriched combustion, closed IGCC
   Development of low cost oxygen supply technology
- Chemical Looping combustion
   Development of low-cost and durable oxygen carriers

## Target for 2030

- For low-pressure gas (CO<sub>2</sub> separation from flue gas, blast furnace gas, etc.) JPY2,000 level/t-CO<sub>2</sub> Required energy 1.5 GJ/t-CO<sub>2</sub> Chemical absorption, solid absorption, etc.
- For high-pressure gas (CO<sub>2</sub> separation from chemical process/fuel gas, etc.) JPY1,000 level/t-CO<sub>2</sub> Required energy 0.5GJ/t-CO<sub>2</sub> Physical absorption, membrane separation, etc.
- Overall review of other processes
   Closed IGCC/Chemical looping, etc.
   JPY1,000 level/t-CO<sub>2</sub>
   Required energy 0.5GJ/t-CO<sub>2</sub>
- <Establishing a CO<sub>2</sub> capture system>
- Realization of an energy-saving, low cost CO<sub>2</sub> capture system that is designed for each CO<sub>2</sub> emission source/usage
- Realization of 10,000 hour continuous operation (to demonstrate the robustness and reliability)

## Target from 2050 Onwards

- <Commercialization of CO<sub>2</sub> capture technology>
- Achieve JPY1,000/t-CO<sub>2</sub> or lower
- Improve the robustness and reliability of CO<sub>2</sub> capture systems
- Optimize CO<sub>2</sub> capture systems according to the emission source and application
- Full-fledged spread of CO<sub>2</sub> capture systems

## **Common technology**

## Explanations on CO<sub>2</sub> capture technologies

Capture technologies	Principle	Application areas	
Chemical absorption	<ul> <li>Chemical reaction between CO<sub>2</sub> and liquid.</li> </ul>	thermal power plants, cement manufacturer, iron and steel production, petroleum refining, chemical production and fossil fuel extraction	
Physical absorption	• Dissolution $CO_2$ into liquid. Efficiency depends on the solubility of $CO_2$ in the absorbent.	thermal power plants(high gas pressure), petroleum refining, chemical production and fossil fuel extraction	
Solid absorption	<ul> <li>Absorption into solid absorbents.</li> <li>Absorbents include porous materials impregnated with amines (for low temperature separation) or other solid absorbents for high temperature separation.</li> </ul>	thermal power plants, cement manufacturer, petroleum refining and chemical production	
Physical adsorption	<ul> <li>Adsorption onto porous solid such as zeolite.</li> <li>Realized by increase and decrease of pressure (i.e. pressure swing) or temperature (i.e. temperature swing).</li> </ul>	thermal power plants, cement manufacturer, iron and steel production, petroleum refining and chemical production	
Membrane separation	<ul> <li>Permeation through a membrane, which has selective permeability for different gas species</li> </ul>	thermal power plants(high gas pressure), petroleum refining, chemical production and fossil fuel extraction	

## **Basic substances**

### Methane Chemistry, etc.

(Until inexpensive Hydrogen can be supplied, methane (CH<sub>4</sub>) will be used instead of CO<sub>2</sub>.)

#### [CH₄→Syngas (1)]

- Established as a commercial process
- Partial oxidation/ATR, dry reforming: There is a room for improvement, such as making the reaction temperature lower, searching suitable catalysts, improving durability, etc.

#### [CH₄→Others]

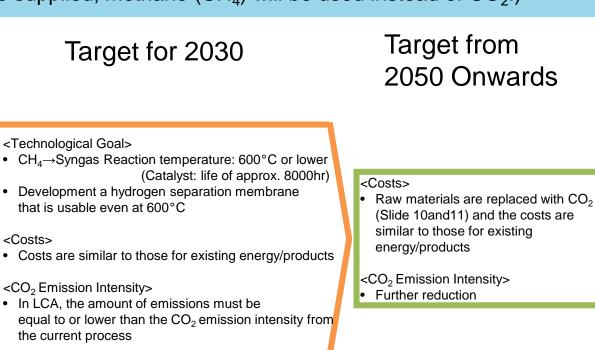
- Separation under high temperature conditions (hydrogen and benzene, etc.)
- Direct synthesis of methanol(2) and of ethylene (3) are still at R& D stage.
- Methane thermal cracking where  $CO_2$ -free hydrogen can be obtained is still at R& D stage (catalyst development, carbon removal/utilization technology)

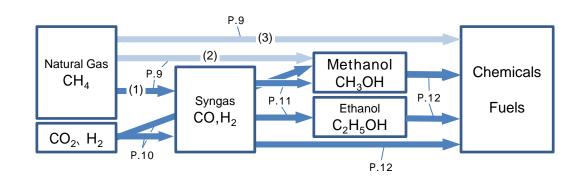
#### [Wastes→Useful Substances]

- Sophisticate a recycling technology that utilizes waste plastics(physical selection of plastics, removal of impurities, halogen-resistant catalysts, etc.)
- Establishment of industrialized process

#### <Other Challenges>

Heat management, equipment costs, development of low-cost oxygenation (such as the utilization of oxygen concurrently produced during electrolysis)





## **Basic substances**

## Technologies to produce syngas containing Carbon Mono-oxide and Hydrogen

#### Thermal Chemistry (catalysts, etc.)

<Technological Challenges>

- Further improvement in current processes (reverse-shift reaction) <Other Challenges>
- Capture and reuse of the CO<sub>2</sub> produced as a byproduct in reaction system <Example of specific efforts>
- Thermal cracking of CO<sub>2</sub> utilizing solar heat

#### Photochemistry (photocatalysts, etc.)

Artificial Photosynthesis (photocatalysts)

- <Technological Challenges>
- Catalyst Development Hydrogen synthesis (photocatalysts) → Reverse shift reaction Direct synthesis of CO

Improvement in conversion efficiency and separation of gas generated <Other Challenges>

- System design of a plant whose commercialization is viable
- Examination and comparison with the current CO production process (methane-derived)

#### Electrochemistry (electrochemical reduction, etc.)

Artificial Photosynthesis (PV-electrochemical cell)

<Technological Challenges>

- Development of a catalyst electrode that is suitable for high current density (improve reaction rate)
- Development of integration technology for catalyst electrodes (improve the current density per unit volume)
- Production of syngas through co-electrolysis (respond to load change, equipment scale)

<Other Challenges>

- System design of a plant whose commercialization is viable
- Examination and comparison with the current CO production process (methane-derived)
- Securing reasonable and stable, large amounts of power derived from renewable energy

Synthesis utilizing organisms (such as microorganisms)

#### • Implement various types of R&D

### Target for 2030

#### <Conversion Efficiency

- (Photochemistry)>
- Solar energy conversion efficiency: 10% achievement

#### <Reaction Rate (Current Density)>

• CO<sub>2</sub> processing speed 6t/yr/m<sup>2</sup> (Achievement of current density 500mA/cm<sup>2</sup> at ordinary temperature/normal pressure, electrolytic efficiency50%) (Electrochemistry) <sup>Note 1</sup>)

#### <Catalysts>

• Further improvement in durability and Reduction in costs

#### (Others)

- Development of renewable energy combined systems
- Development of hybrid systems (Photo + Electricity, etc.)
- Sector coupling: Demonstrate a case where CO is used as a reducing agent for steelmaking

## Target from 2050 Onwards

<Conversion Efficiency (Photochemistry)> Further improvement of conversion efficiency

<Reaction Rate (Current Density)> CO<sub>2</sub> processing speed 11 t/yr/m<sup>2</sup> (Achievement of current density 1000mA/cm<sup>2</sup> at ordinary temperature/normal pressure, electrolytic efficiency 50%) (Electrochemistry) <sup>Note 1</sup>)

#### (Others)

 Synthesis that utilizes thermal chemistry/photochemistry/ electrochemistry/organisms is the best mix of various reactions/technologies.

Note1) Estimate under the following conditions: 100MW plant, availability factor:16.3%, and JPY 2/kWh.

Source of the available factor: Materials owned by ANRE (Agency for Natural Resources and Energy)

Note2) Supplying inexpensive CO<sub>2</sub> free Hydrogen is important

## **Basic Substances**

### Technologies to produce Methanol, etc.

#### Thermal Chemistry(catalysts, etc.)

 $[\operatorname{CO}_2 \to \operatorname{Methanol}]$ 

- <Technological Challenges>
- Reaction at low temperature Catalyst development/improvement in catalyst's conversion rate/selectivity
- · Separation/removal of the water arising from the reaction
- Direct utilization of low quality exhaust gas (at a research stage) Measures against deterioration/improvements of durability of catalysts
   Other Challenges>
- Examination and comparison with the current practical process (reaction through syngas)
- Utilization of CO<sub>2</sub> in existing methanol production equipment

 $[Syngas \rightarrow Methanol (or DME)]$ 

<Technological Challenges>

- Improvement of yields in methanol production
- A system for concurrent production of methanol and DME where syngas is used as a raw material
  - (production adjustment technique)

#### Photochemistry (photocatalysts, etc.)

Electrochemistry (electrochemical oxidation/reduction, etc.)

Synthesis utilizing organisms(such as microorganisms)

#### Implement various types of R&D

<Technological Challenges>

- Direct synthesis of formic acid/methanol(by utilizing the protons in water)
- Improvement in reaction rate and efficiency

<Other Challenges>

• Securing reasonable and stable, large amounts of power derived from renewable energy (in the case of utilizing electricity)

<Specific Practical Example>

Demonstration of integrated bioethanol production from syngas (derived from waste incineration facilities) using microorganisms (The technology to be established by 2023: Goal 500 ~ 1,000kL/y scale demonstration to be implemented)

some processes require no further hydrogen

# Target for 2030 Target from 2050 Onwards

<Common Challenges>

Reduction in process cost

#### <Others>

- Development of renewable energy combined systems
- Development of hybrid systems (Photo + Electricity, etc.)
- Considering large-scale methanol supply chain
- Apply the technology to existing production systems/secure affinity
- <Challenges to be taken up when methanol is utilized as a raw material>
- Demonstrate the technology for methanol to be used in an actual environment
- Expand mixed utilization of existing fuels and methanol as well as the mixed ratio

#### <Common Challenges>

• Further reduction in process cost

#### <Expected Cost>

• The expected costs are roughly equal to those incurred for the product synthesized from natural gas-derived methanol

## Chemicals

Technologies to produce commodity chemicals (Olefins, BTX, etc.)

#### <Technological Challenges>

[MTO-olefin] (production plants exist)

Developing catalysts (improvement in conversion rate/selectivity)

E.g., Controlling generation ratio of Ethylene, propylene, butane, etc.

• Countermeasures against catalyst poisoning (controlling carbon precipitation)

[MTA-BTX] (R&D projects exist)

• Developing catalysts (improvement in conversion rate/selectivity)

E.g., Controlling generation ratio of Benzene, toluene, xylene, etc.

Regarding MTO and MTA, methanol derived from coal is implemented or under implemented in China.

#### [Syngas→olefin, BTX]

Basic research level

Developing catalysts (improvement in conversion rate/selectivity)

E.g., Controlling generation ration of Benzene, toluene, xylene, etc.

Suppression of the generation of CO<sub>2</sub> and methane

#### [MTO-olefin]

#### <Catalyst>

Establish C2-C4 selective synthesis technology

Target for 2030

- Further improvement in yield and Control of selectivity
- Establish a small-pilot-scale process

#### [MTA-BTX]

<Catalyst>

• Further improvement of yield and control of selectivity

#### [Syngas -> Olefin, BTX]

<Catalyst>

 Further improvement of yield and control of selectivity

<CO2 Emission Intensity>

• In LCA, the amount of emissions must be equal to or lower than the CO<sub>2</sub> emission intensity from the current process

## Target from 2050 Onwards

#### <Expected Cost>

• The costs are similar to those for existing energy/products

#### <CO<sub>2</sub> Emission Intensity>

 In LCA, the amount of emissions must be equal to or lower than half of the CO<sub>2</sub> emission intensity from the current process

## Chemicals

### Technologies to produce oxygenated compounds

<Technological Challenges>

- Reduce cost in the current process or for commercialization (polycarbonate synthesis, etc.)
- Further reduction of CO<sub>2</sub> emissions
- Reduction in production costs

Basic research level, under low TRL Process (acrylic acid synthesis, etc.)

- Catalyst development (improvement in conversion rate/selectivity)
- Realization of low LCA for reaction partners (such as utilizing biomass/waste plastics, etc.)

<Other Challenges>

 Considering another CO<sub>2</sub> storage technique based on chemicals (such as oxalic acid, etc.)

## Target for 2030

## Target from 2050 Onwards

<Expected Cost>

• The costs are similar to those for existing energy/products

<CO<sub>2</sub> Emission Intensity>

 In LCA, the amount of emissions must be equal to or lower than the CO<sub>2</sub> emission intensity from the current process <Expected Cost>

• Further reduction in costs

#### <CO<sub>2</sub> Emission Intensity>

 In LCA, the amount of emissions must be equal to or lower than half of the CO<sub>2</sub> emission intensity from the current process

Oxygenated compounds include (in alphabetical order):

acetic acid, acetic acid ester, acrylic acid, ethanol, ethylene glycol, oxalic acid, polyamide, polycarbonate, polyester, salicylic acid, urethane, etc.

## **Chemicals**

## Technologies to produce biomass-derived chemicals

#### <Technological Challenges>

(Cellulose-type biomass)

- Low cost, effective pretreatment technique (separation of cellulose, lignin, etc.)
- Establish the related techniques such as dehydration/drying, removal of impurities, etc.
- Production process of high-value added chemicals from non-edible biomass
- Screening and culture techniques for new microorganisms resources
- Utilization of biotechnology (Genome editing/synthesis), establishment of separation/purification/reaction process techniques
- Fermentation technology and catalyst technology that are not susceptible to impurities
- Development of effective materials conversion technologies for biomass materials
- High functionality in biomass-derived chemicals (adding marine biodegradable functions, etc.)

#### <Other Challenges>

- Establishing integrated production processes (securing production scale, stability in quality, etc.)
- Expanding the scope of target products including derivatives (oxygenated compounds→olefin, etc.)
- Expanding the scope of application of biomass-derived chemicals and verify their economic performance
- Establishing an effective collection system for biomass materials
- Standardization of biomass-derived chemicals/intermediates

Target for 2030

#### <Expected Cost>

 The costs are similar to those for existing energy/products

#### <CO<sub>2</sub> Emission Intensity>

• In LCA, as compared to alternative petrochemical products (such as oxygenated compounds, etc.), the amount of emissions must be equal to or lower than half of the CO<sub>2</sub> emission intensity from the current process

#### <Others>

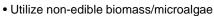
- Diversification and high functionality of biomass-derived chemicals (Controlling marine biodegradable functions, etc.)
- Hydrogen is necessary in hydrogenation treatment

## Target from 2050 Onwards

 Large-scale production (geographically-distributed chemicals production that utilizes papermaking infrastructure/ agriculture and forestry/wastes, etc.)

#### <CO<sub>2</sub> Emission Intensity>

- · In LCA, as compared to alternative petrochemical products (such as olefin, etc.), the amount of emissions must be equal to or lower than half of the CO<sub>2</sub> emission intensity from the current process
- Introduction into global markets (Marine biodegradable plastics : JPY 850 billion (Global market share of Japan: 25%))



Bio power generation (ultimately, BECCS)

Diversification of biomass chemicals/fuels

- Image of expansion
- Utilize edible biomass (mainly, ethanol and amino acid) Utilize oils and fats
- · Bio and waste power generation
- Synthesize high-value added chemicals (functional chemicals)

Such technological development is also common to that in fuel sector (bioethanol, etc.) Cultivation and capturing biomass technologies include marine use as well (fuel sector as well)

## **Fuels**

## Technologies to produce liquid fuel (1) \*Microalgae Biofuel (Jet Fuel/Diesel)

#### <Technological Challenges>

- (Microalgae→Biojet fuel/Biodiesel)
- Improve productivity (culture system/ gene recombination)
- Low cost, effective pretreatment technique
- Establish the related techniques such as dehydration/drying, oil extraction, removal of impurities, etc.
- Develop the technology for utilizing oils/fats residues
- Scale-up (from bench-scale to pilot-scale, followed by demonstration level)
- Large-scale technological demonstration
- Pursuit of cost reduction

#### <Other Challenges>

- Expanding the scope of application and verify economic performance
- Establishing an effective collection system for raw materials

#### <Expected Cost>

 Bio-jet Fuel: costs: similar to those for existing energy/products, JPY 100-200/L (Currently, JPY1600/L)

Target for 2030

#### <Production Rate>

• 75 L-oil/day ha (Currently, 35 L-oil/day ha)

#### <CO2 Emission Intensity>

 With regard to biojet fuels, in LCA, as compared to existing jet fuels, the amount of emissions must be equal to or lower than half of the CO<sub>2</sub> emission intensity from the current process

#### <Others>

- Compliance with fuel standards
- Scale up to the demonstration level and establish the supply chain
- Expand mixed utilization of the liquid fuel and an existing fuel as well as the mixed ratio
- Since hydrogen is used in relatively small amounts for oil reforming, the presence of CO<sub>2</sub> free hydrogen increases the GHG reduction impact

## Target from 2050 Onwards

#### <Expected Cost>

• Further reductions in costs

#### <CO<sub>2</sub> Reduction Amount>

 Must contribute to 50% CO<sub>2</sub> reduction relative to that for 2005 in aviation sectors

(FYI) If a biojet fuel with a greenhouse gas emission reduction rate of 50% continues to be introduced at 100 thousand kL/yr, a  $CO_2$  reduction of 123 thousand t/yr will be achieved.

## **Fuels**

## Technologies to produce liquid fuel (2) \*CO<sub>2</sub>-derived fuel or Biofuel (excluding microalgae-derived fuels) (such as methanol, ethanol, diesel, jet, DMC, OME, etc.)

#### <Technological Challenges>

- Improvement in FT Synthesis (current process) (Improvement in conversion rate/selectivity)
- Improvement in other synthetic reaction (current process)

#### <Other Challenges>

 System's optimization (Renewable energy introduction (E-Fuel))

#### <Specific Practical Example>

 Demonstration of integrated bioethanol production from syngas (derived from waste incineration facilities) using microorganisms (The technology to be established by 2023: Goal 500-1,000kL/y scale demonstration to be implemented)

some processes require no further hydrogen

## Target for 2030

<CO<sub>2</sub> Emission Intensity>

 In LCA, the amount of emissions must be equal to or lower than the CO<sub>2</sub> emission intensity from the current process

#### <Other Challenges>

- Wondering what impact a CO<sub>2</sub>-derived fuel may have on the regulations/ device/equipment on which naphtha-/crude oil-derived fuels had no effect
- Demonstrate the technology in an actual environment
- Expand mixed utilization of the liquid fuel and existing fuels as well as the mixed ratio

## Target from 2050 Onwards

#### <Expected Cost>

• The costs are similar to those for existing energy/products

#### <CO<sub>2</sub> Emission Intensity>

 In LCA, the amount of emissions must be equal to or lower than half of the CO<sub>2</sub> emission intensity from the current process

Costs for biofuels and target for CO2 emissions, the same as biomass derived chemicals and microalgae biofuels attempt to reduce the cost equivalent to those existing energy/products in 2030 as well as in LCA the amount of emissions must be lower than half of the CO2 emissions intensity from the current process.

## **Fuels**

### Technologies to produce gas fuel (Methane)

<Technological Challenges> Existing Techniques (Sabatier Reaction)

- Long lasting of catalysts
- Thermal management (utilizing the generation of heat)
- Activity management
- Considering scale-up

R&D of Innovative Technology (co-electrolysis, etc.)

[Power to Methane]

- Production of electrolytic methane through coelectrolysis (utilization as city gas, etc.)
- Integrate the synthesis/power generation of electrolytic methane that utilizes CO2
- Improvement of efficiency

<Other Challenges>

- System's optimization (introducing renewable energy)
- Upsizing/cost reduction
- Equipment cost

#### <Specific Practical Example>

- Commercial scale (125Nm<sup>3</sup>/h) demonstration that utilizes CO<sub>2</sub> contained in exhaust gas from a cleaning plant
- Development of basic technology towards practicalscale (60 thousand Nm<sup>3</sup>/h) demonstration of introducing city gas that utilizes CO2 emission from coal fired thermal power plants

### Target for 2030

#### <Expected Cost>

• Reduction in costs for CO<sub>2</sub> derived CH<sub>4</sub>

#### <CO<sub>2</sub> Emission Intensity>

 In LCA, the amount of emissions must be equal to or lower than the CO<sub>2</sub> emission intensity from the current process

#### <Others>

- Demonstrate injection into gas introduction pipes
- Develop sales channel/use application
- Expand mixed utilization of the gas fuel and an existing fuel as well as the mixed ratio

## Target from 2050 Onwards

#### <Expected Cost>

• The costs are similar to those for existing energy/products

#### <CO<sub>2</sub> Emission Intensity>

 In LCA, the amount of emissions must be equal to or lower than half of the CO<sub>2</sub> emission intensity from the current process

## Minerals

### Technologies to produce carbonates, concrete products and concrete structures, etc.

#### <Technological Challenges>

- Separation of effective components (Ca or Mg compounds) from industrial byproducts (such as iron and steel slag, waste concrete, coal ash, etc.) and/or mine tailings, produced water (e.g., brine) etc. (including the treatment of byproducts arising from the separation process)
- Energy-saving of the pretreatment (for example, comminution of effective components) that helps to enhance the reactivity with CO<sub>2</sub> (dry process)
- Energy-saving in wet process (inexpensive treatment for waste water containing heavy metals, etc.)
- Development of inexpensive aggregates, admixtures, etc.
- Scale up

<Energy required to mineralize 1 ton of CO<sub>2</sub> >

500 kWh/t-CO<sub>2</sub> (utilizing iron and steel slag, dry process)

#### <Other Challenges>

- Establish a supply system from CO<sub>2</sub> emission sources to mineralization process (optimized to net CO<sub>2</sub>-fixiation and economic performance)
- Expand the scope of application and verify economic performance (development and demonstration of the technologies designed to utilize carbonates – verify the scope of application to concrete products, develop high-value added articles such as luminous materials, etc.)
- Long-term evaluate the performance as a civil-engineering/ building material as well as organize standards/guidelines

#### <Specific Practical Example>

 Development of a technology that is used to convert unused highly reactive industrial byproducts into carbonates (e.g., coal ash), which pretreated by energy saving process

Even now, iron and steel slags and coal ash are used as materials for concrete but not in the form of carbonates

### Target for 2030

#### <Expected Cost>

 Road curb blocks: costs are similar to those for existing energy/products

#### <Energy required to mineralize 1 ton of CO<sub>2</sub>>

200 kWh/t-CO<sub>2</sub> (regardless of a raw material and reaction process)

#### <CO<sub>2</sub> Utilization>

 CO<sub>2</sub> mineralization must be applied to ~10% of iron & steel slag and coal ash

#### <Others>

- Large-scale demonstration
- · Pursuit of cost reduction
- · Survey on appropriate sites within/outside the country
- Promotion of demands by providing some incentive (such as procurement for a public work project, etc.)

#### <Specific Practical Example>

 Expand raw materials (Coal ash, biomass mixed combustion ash, waste concrete, etc. → Iron and steel slag, mine tailings, produced water (e.g., brine) utilization (lye water), etc.)

## Target from 2050 Onwards

#### <Expected Cost>

 Other products: The costs are similar to those for existing energy/products

#### <CO<sub>2</sub> Utilization>

- CO<sub>2</sub> mineralization must be applied to ~50% of iron & steel slag and coal ash
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steel slag and coal ash

## Important points for Carbon Recycling Technologies

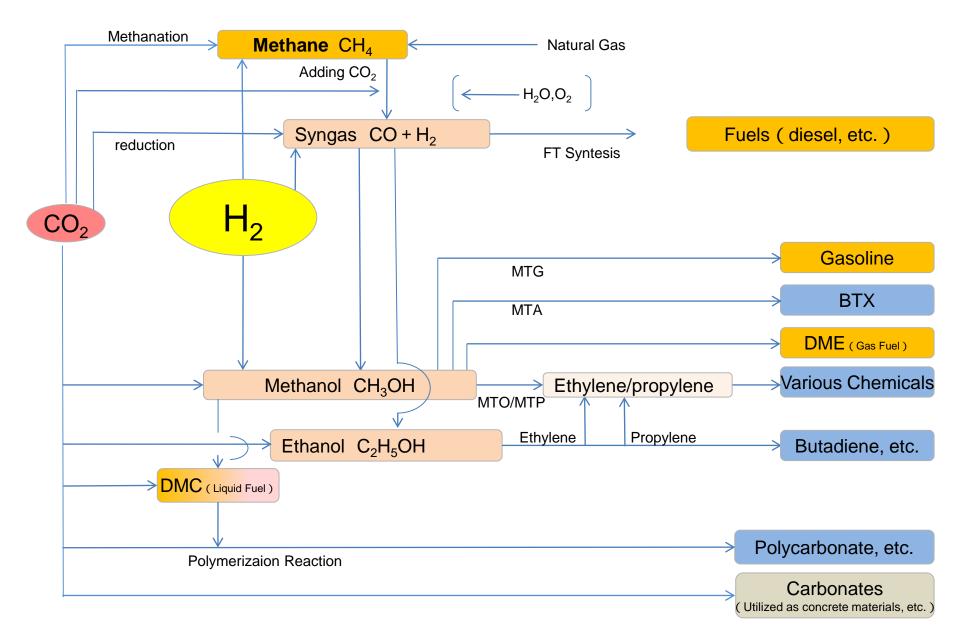
In order to effectively progress R&D in Carbon Recycling technologies to address climate change and security of natural resources, the following points need to be considered.

**ü** Inexpensive CO<sub>2</sub> free Hydrogen is important for many technologies

- Under the hydrogen and fuel cells strategy roadmap in 'Hydrogen Basic Strategy', the target at costs at delivery site for 2050 is JPY 20/Nm<sup>3</sup>
- While the problem of hydrogen supply remains, 1) R&D for biomass and other technologies not dependent on hydrogen should be continue, 2) CH<sub>4</sub> (methane) should be used in place of hydrogen until the establishment of a cheap hydrogen.
- **ü** Using zero emission power supply is important for Carbon Recycling
  - **ü** Conversion of a stable substance, CO<sub>2</sub>, into other useful substance will require a large amount of energy.
- Life Cycle Analysis (LCA) perspective is critical to evaluate Carbon Recycling technologies.
- Reducing the costs for capturing CO<sub>2</sub> will positively feedback into Carbon Recycling.

## Reference

## Flowchart for CO<sub>2</sub> Utilization (for chemicals/fuels/carbonates)



### Flowchart: CO<sub>2</sub> Utilization (for Bio-derived fuels/chemicals)

